

Calciner CFD modelling



An equipment designer's perspective

Damien Grévain and Sam Zakrzewski, Fluid Dynamics specialists, Cement division



One Source

Fluid Dynamics Specialists in Cement Division

	Damien Grévain		Sam Zakrzewski	
Started at FLSmidth	2013		2008	
Fluid dynamics and CFD experience	+14 years		+15 years	
Expertise in	Multi-phase flows, Reacting flows, Particle laden flows			
and	Combustion design		Experimental fluid dynamics HPC systems	
Education	M.Sc. in Industrial Thermal System Engineering from IUSTI Marseille, France - 2001		Ph.D. in Mechanical Engineering from University of New South Wales Sydney, Australia - 2002	

A One-source supplier to the global minerals and cement industries

- ▼ A **leading supplier** of equipment and services to the **global**
 - ▼ **minerals** (100+ years of experience)
 - ▼ **cement industries** (133 years of experience)

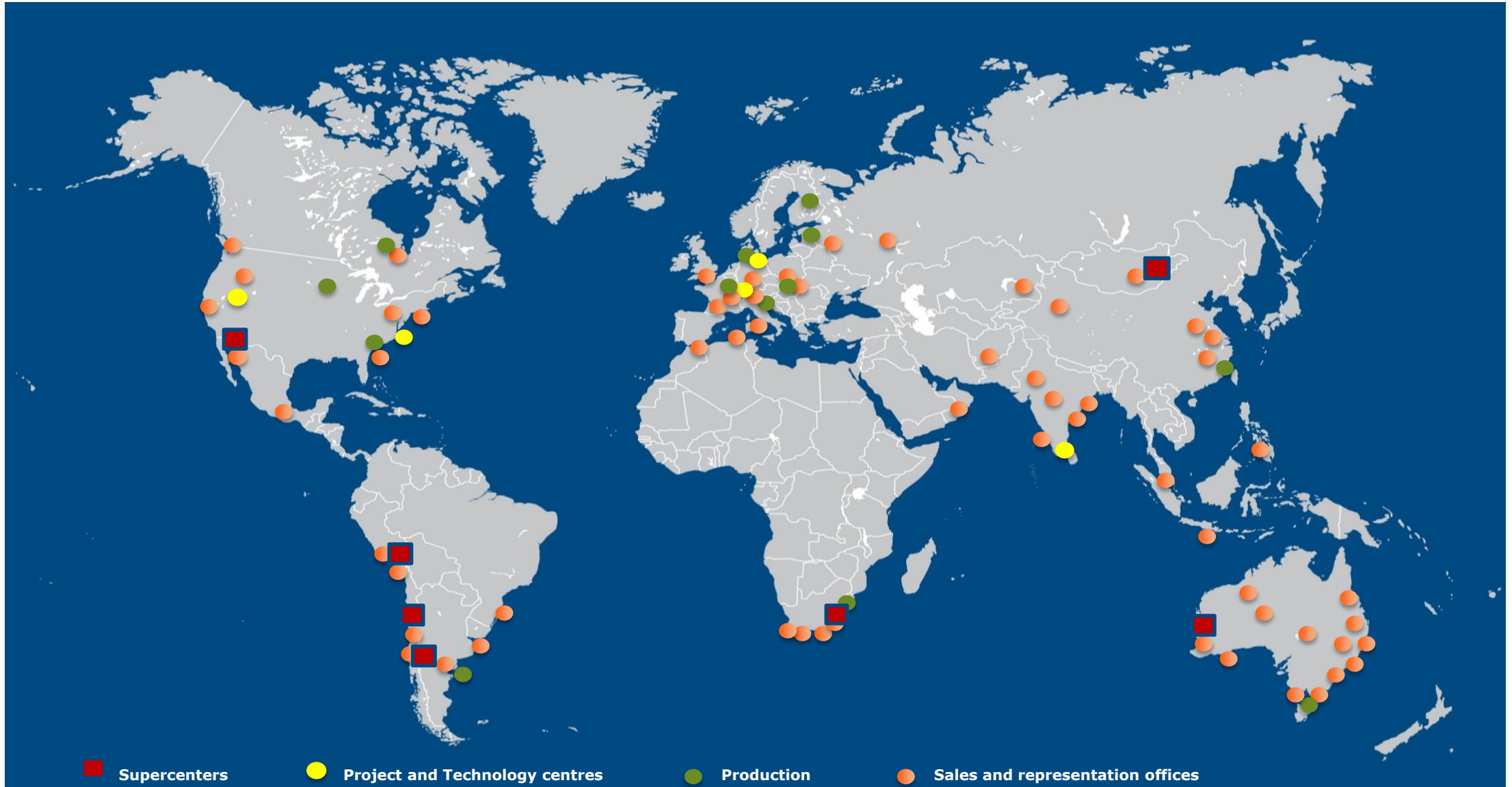
- ▼ FLSmidth **supplies everything from single machine units to complete minerals and cement flow sheets** including associated services

- ▼ FLSmidth primary focus industries:

- ▼ **Coal**
- ▼ **Iron ore**
- ▼ **Fertilizers**
- ▼ **Copper**
- ▼ **Gold**
- ▼ **Cement**



Global reach with presence in 50+ countries



Product Portfolio

Cement



EV Hammer Impact Crusher

Stacker/reclaimer

ATOX mill

MAAG Gear

Pfister feeder

ILC Preh



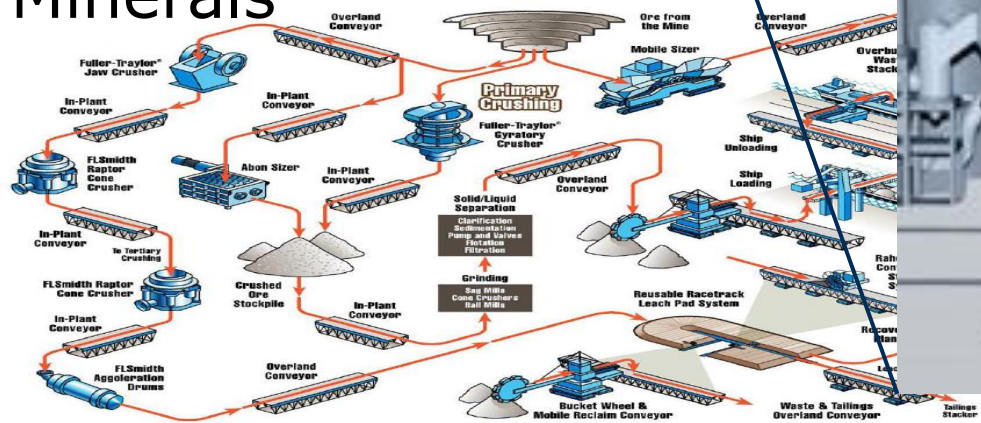
Automation control systems

OK mill

Ventomatic packing equipment



Minerals

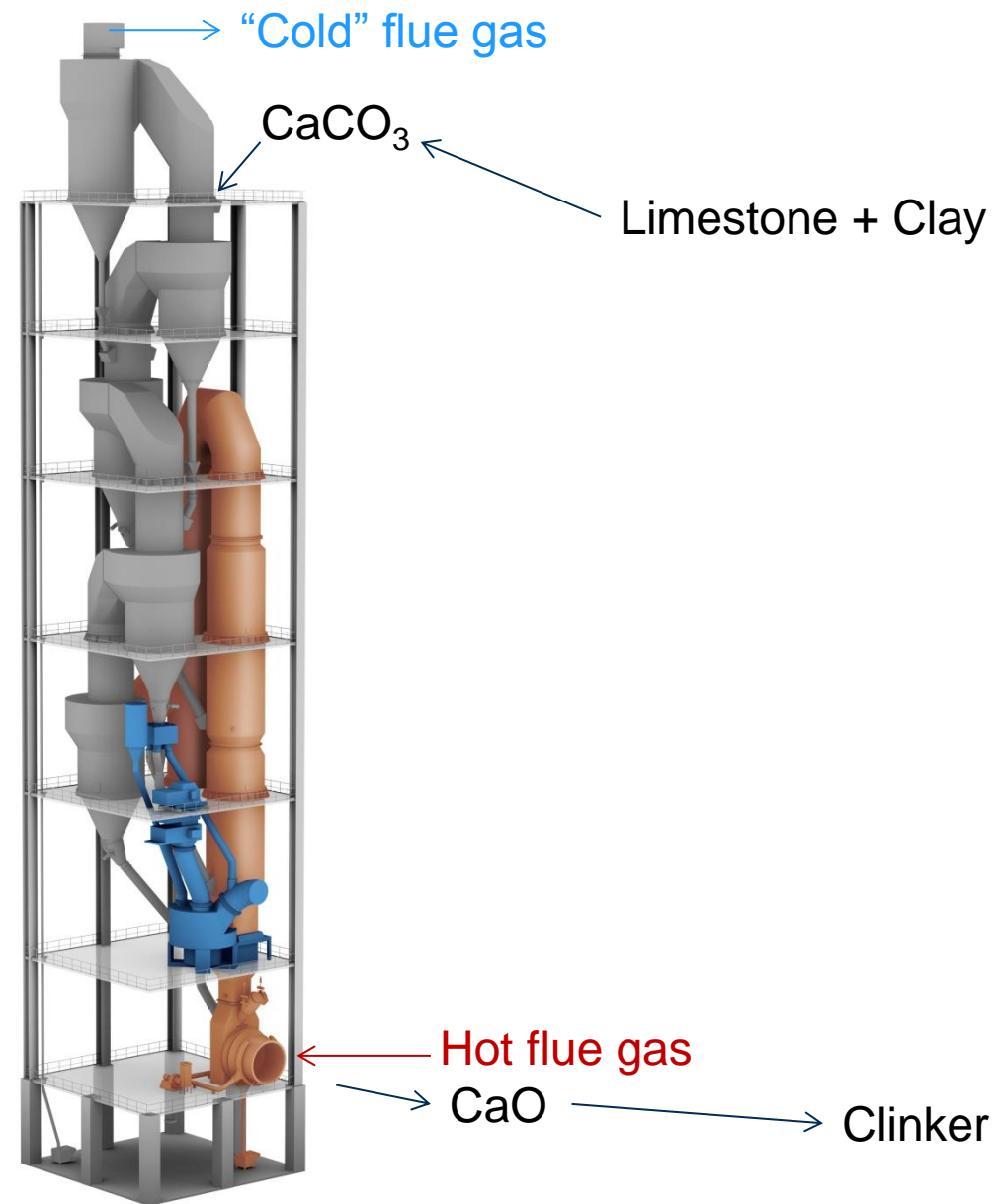


Cement Production Pre-Calciner



Endothermic reaction

1782 kJ/kg CaCO_3



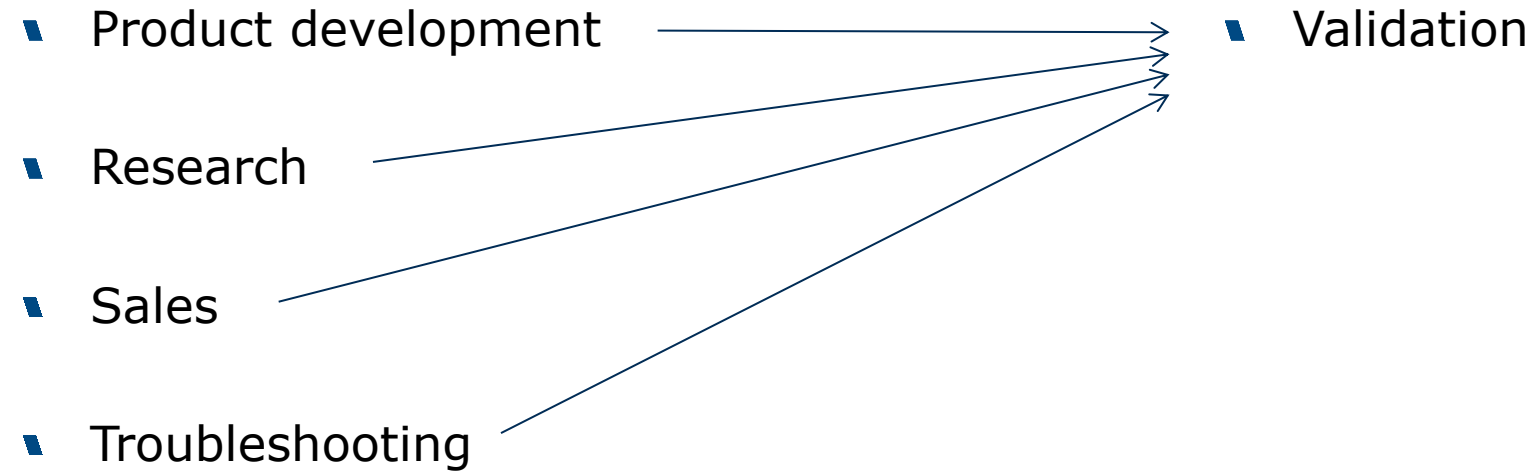
Calciner modelling

What are we investigating?

- Temperature profile
- Gas velocity profile and streamlines
- Mixing
- Meal fall through
- By-pass
- Particle residence time
 - Meal
 - Solid fuel
- Fuel burnout
- Alternative fuel combustion
- Calcination degree

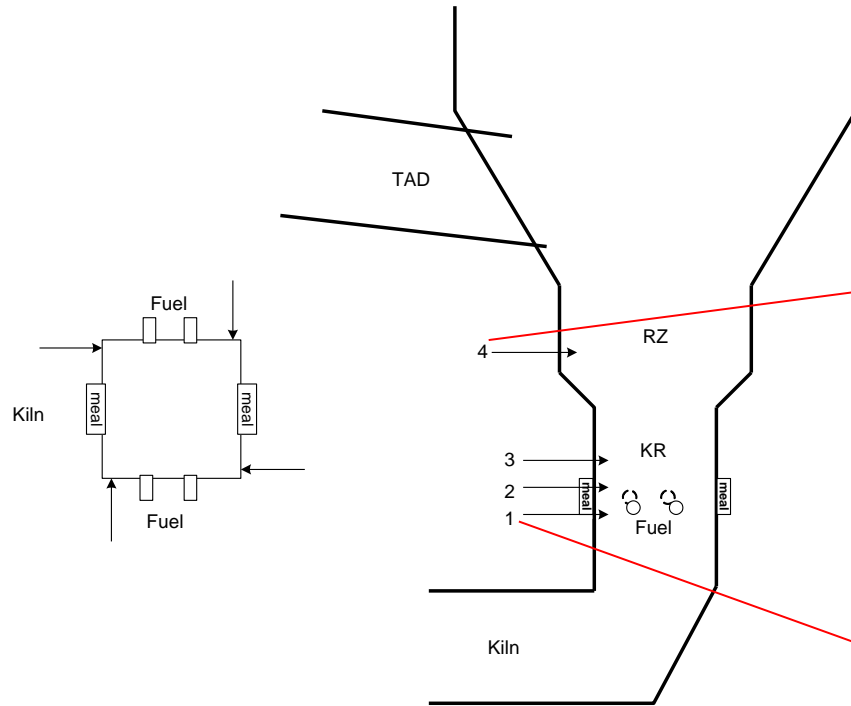
Calciner modelling

Why?



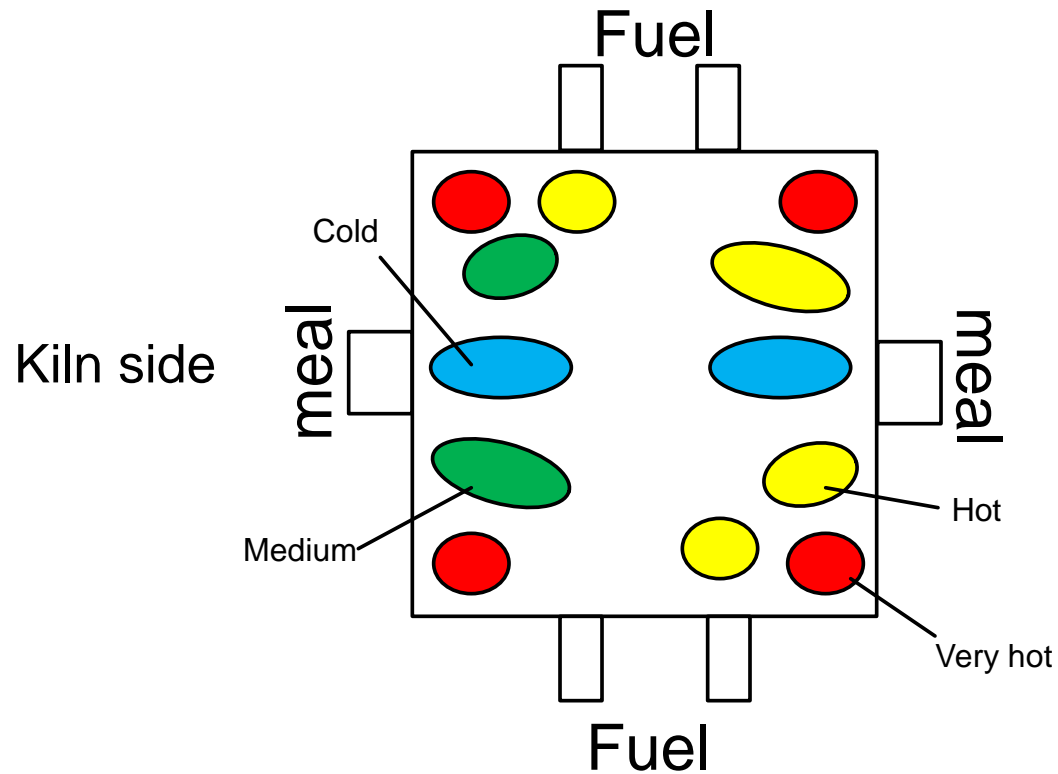
Comparison with measurements Industrial conditions

- Location of temperature mapping



Temperature in riser Industrial conditions

Measurements

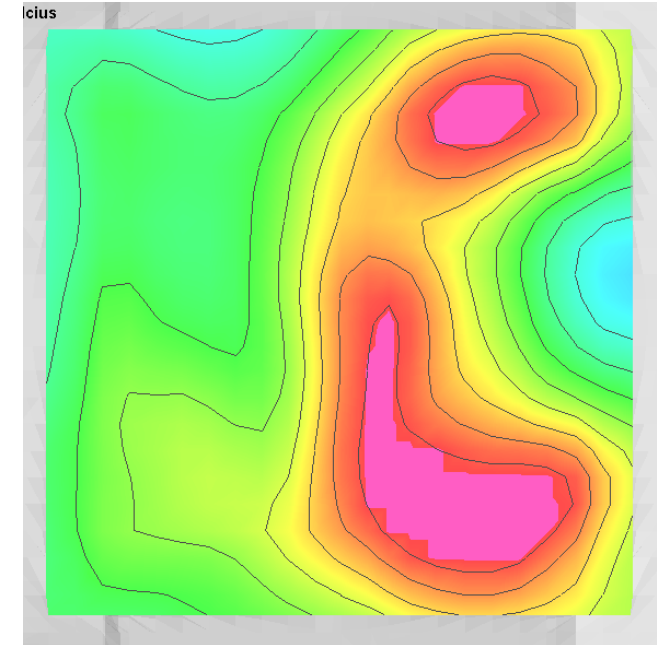
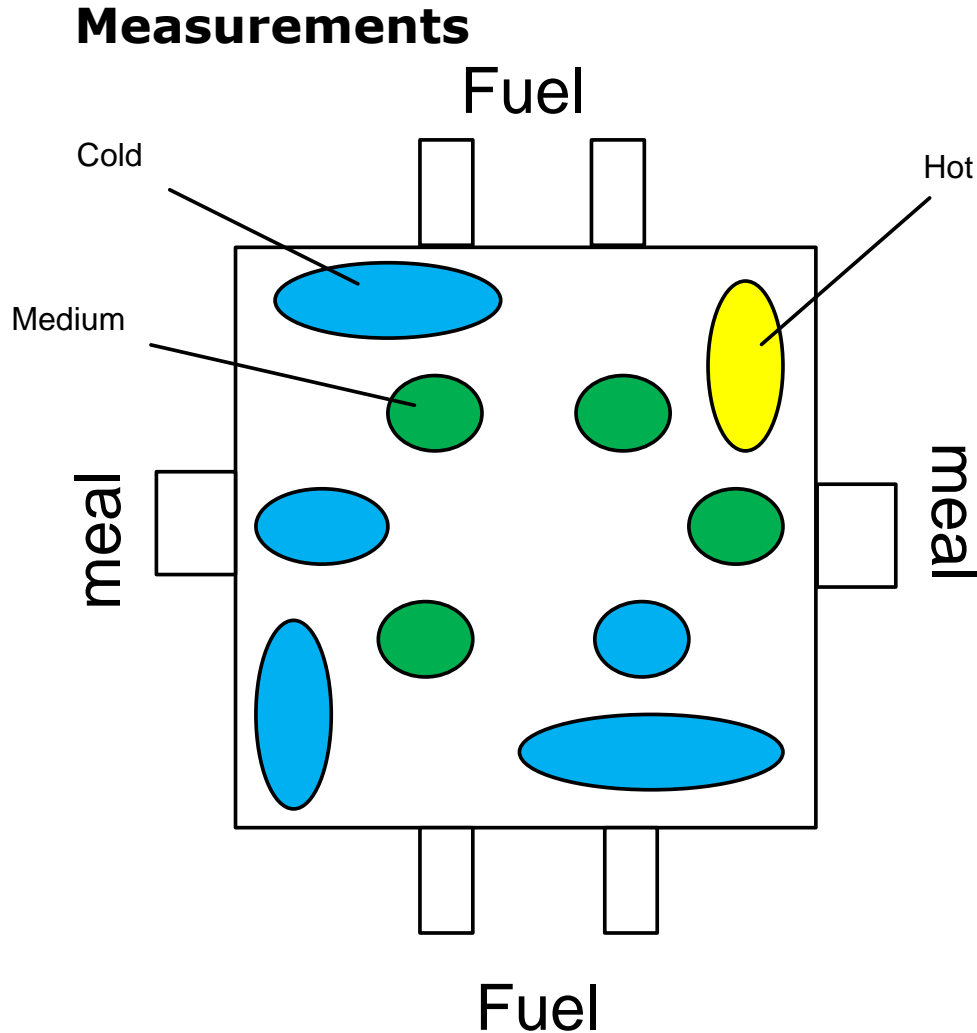


Basecase EMMS - VR 17.0.1



Temperature in calciner bottom duct Industrial conditions

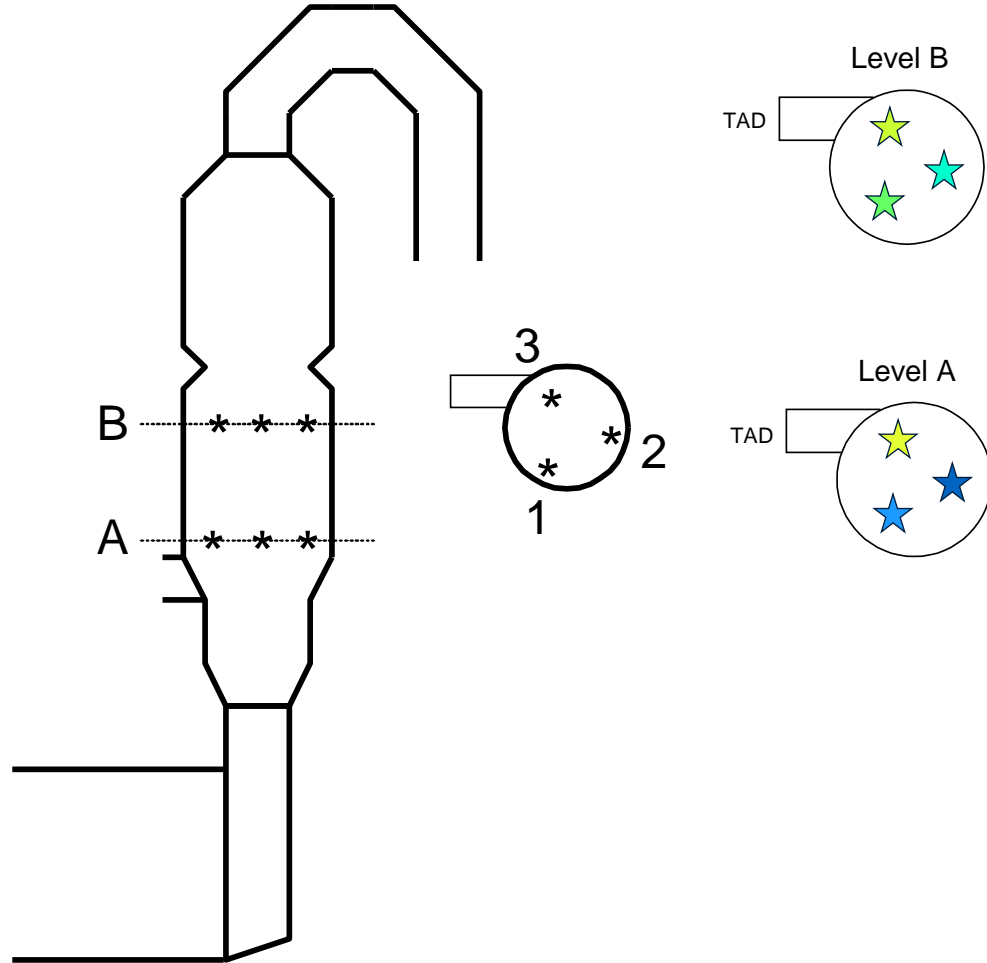
Basecase
EMMS - VR 17.0.1



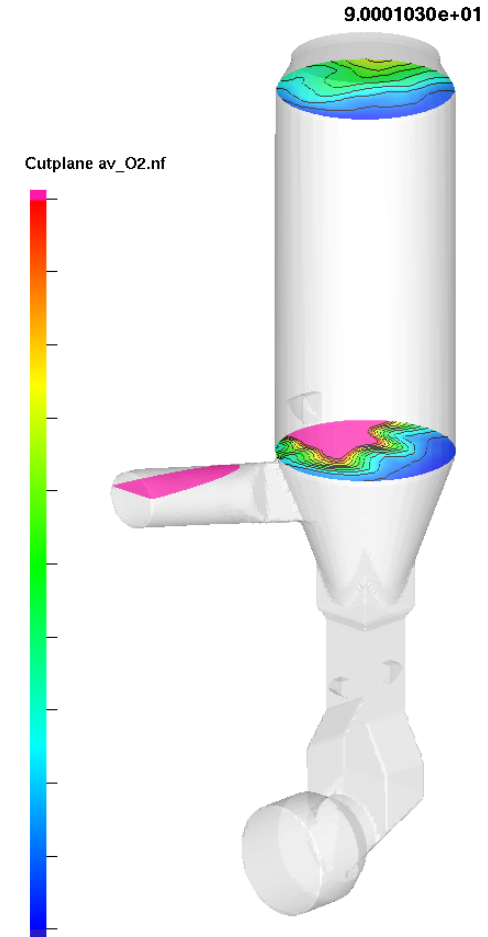
Location of oxygen measurements in calciner

Industrial conditions

Measurements



Basecase EMMS - VR 17.0.1



Meal streams in industrial conditions

General observation from model

Wen-Yu in VR 17

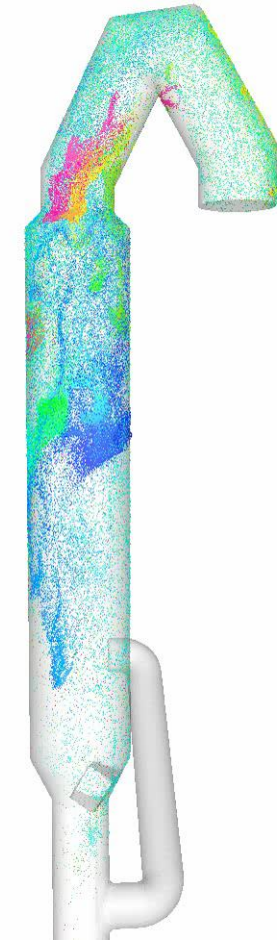
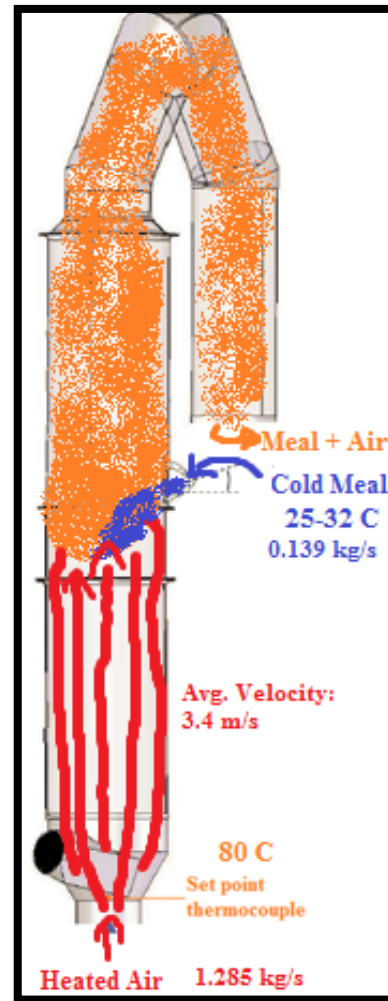
- Meal stream out of spreader box tends to keep close to walls and gather at the bottom of the cone
- Meal falls through riser

EMMS in VR 17

- Meal stream penetrates better across the calciner and achieves much more meal suspension and dispersion
- Less meal falls through riser

Lab scale measurements

- Cooperation with:
 - DTU KT CHEC
 - MiCeTec
- Test centre
- Scaled down industrial calciner 1:12



Lab scale measurements

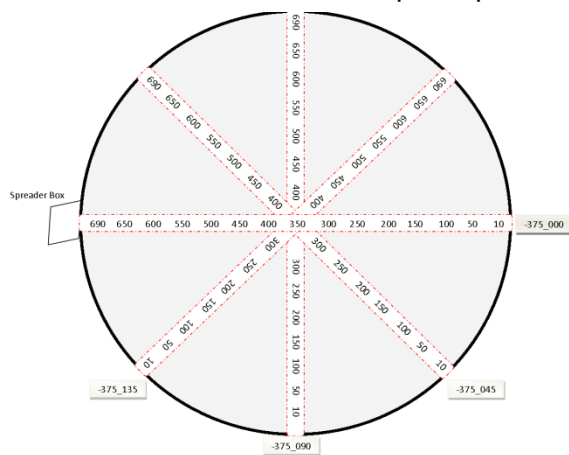
Velocity profile

Single Phase

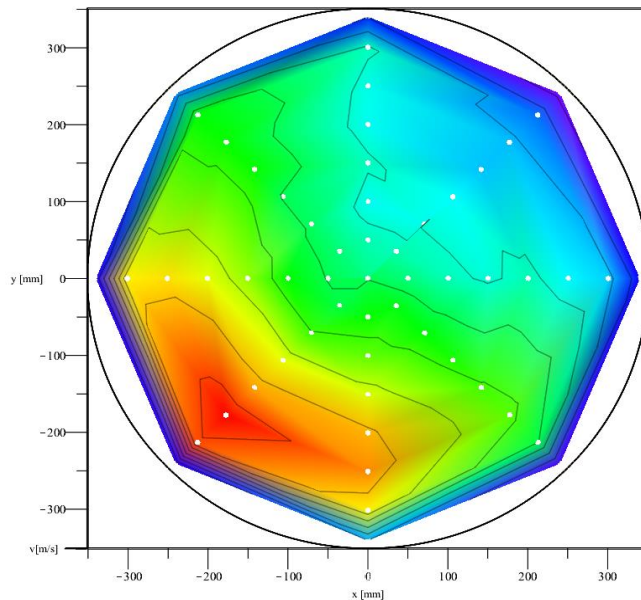
- Upflow velocity with Anemometer



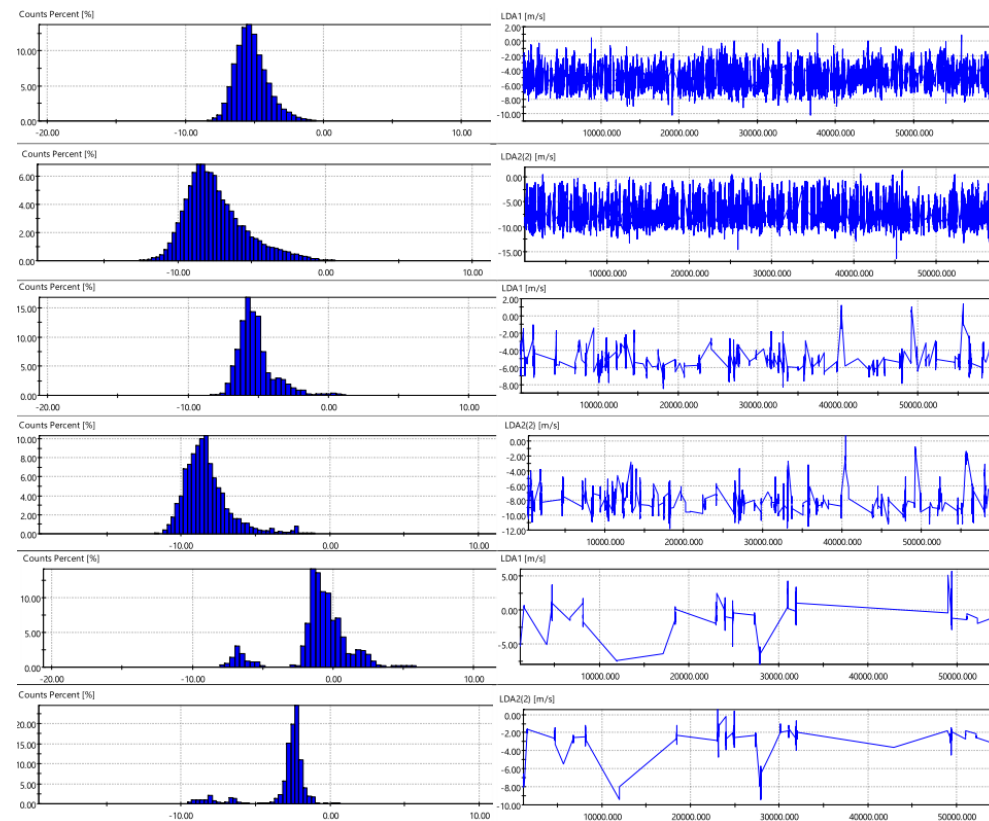
- 375 mm below the top of spreader box



- 60 points measured

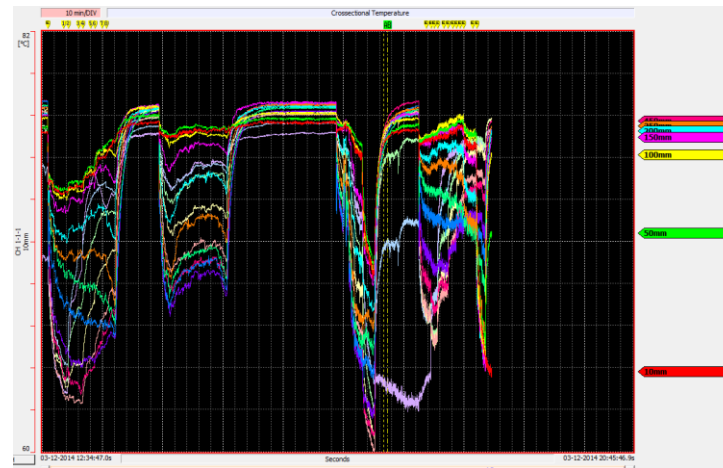
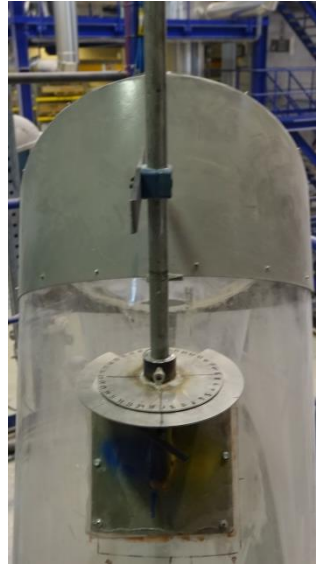


Multi Phase



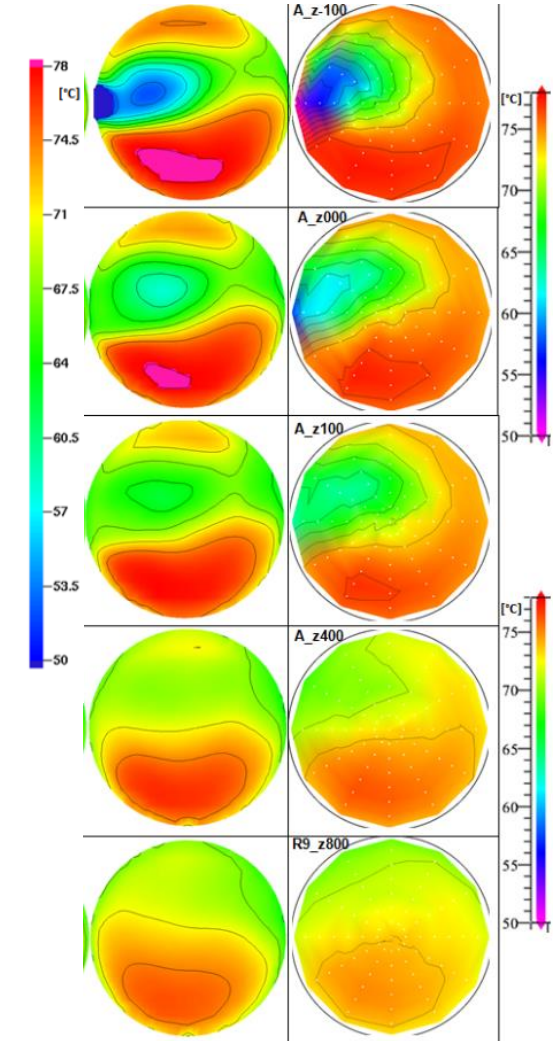
Lab scale measurements

Temperature profile



Computation
EMMS

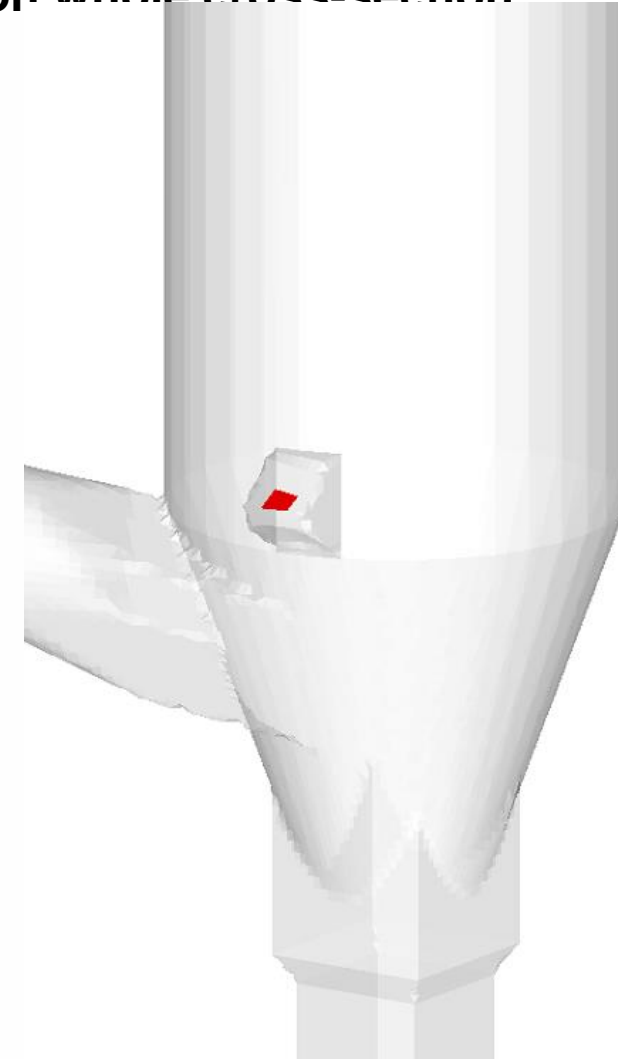
Experiment



Define Boundary Conditions

Meal flow in pipes

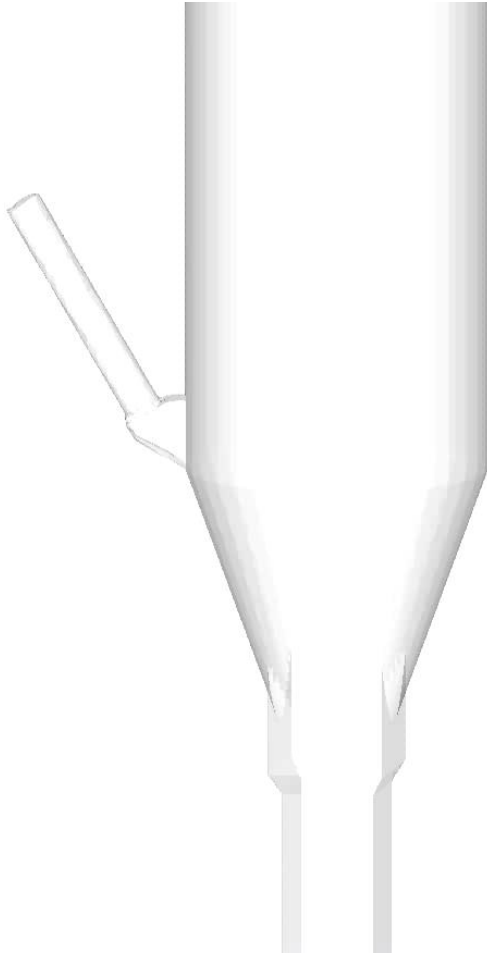
VR 16.0.5 / Wen-Yu
Meal pipe removed
Meal pipe included
BC on few cells
BC on whole cross-section



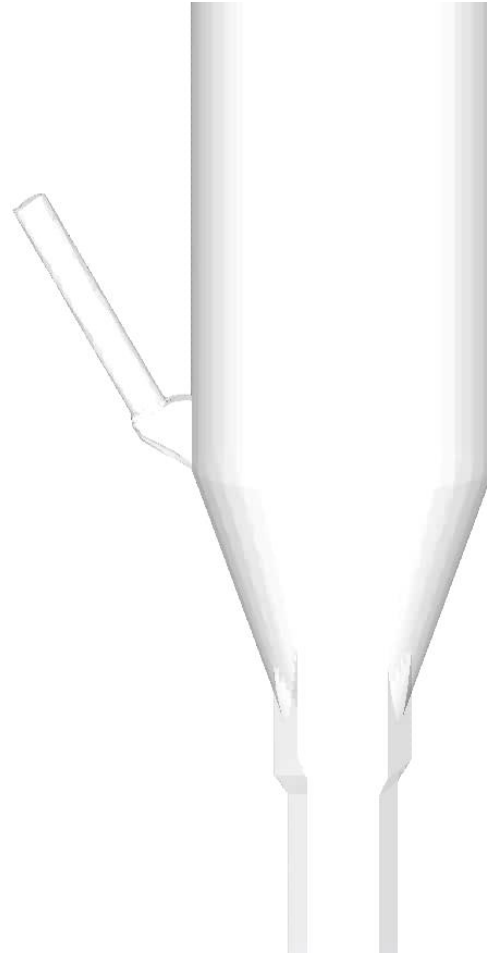
Meal flow in pipes

VR 17.0.3 / EMMS – Different results

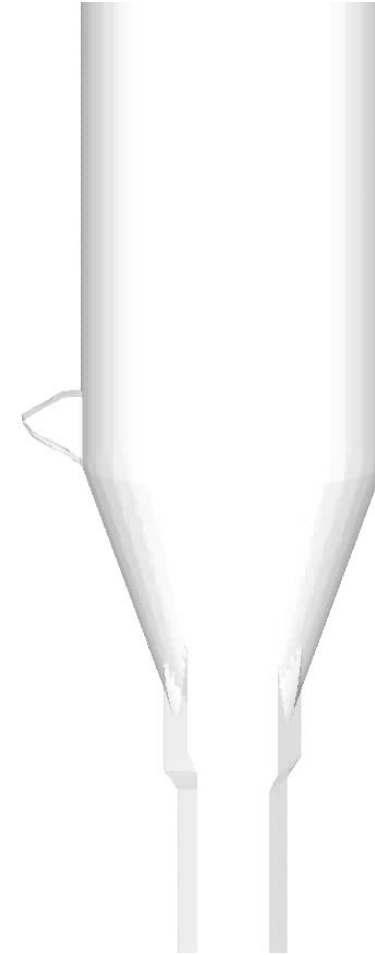
BC on whole cross-section



BC on 4 cells

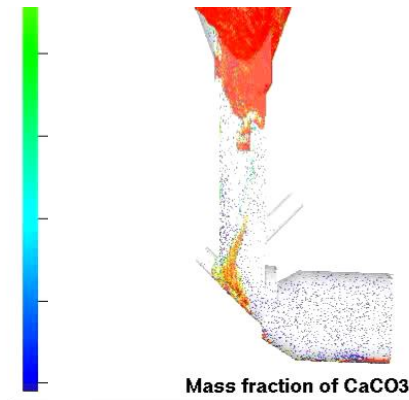
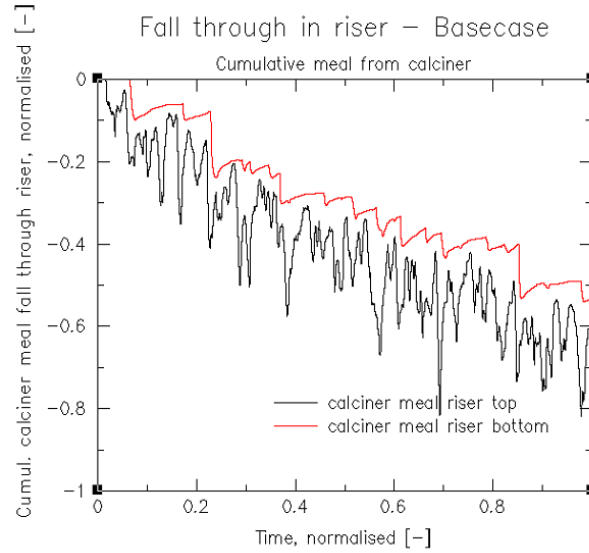
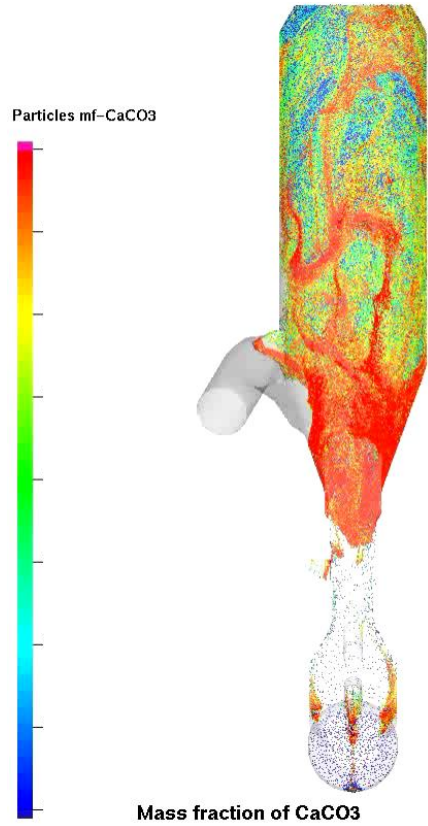


BC on spreader box: 4 cells

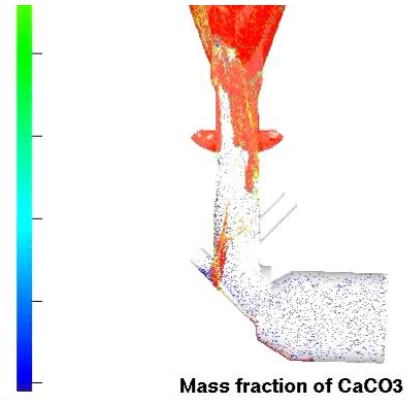
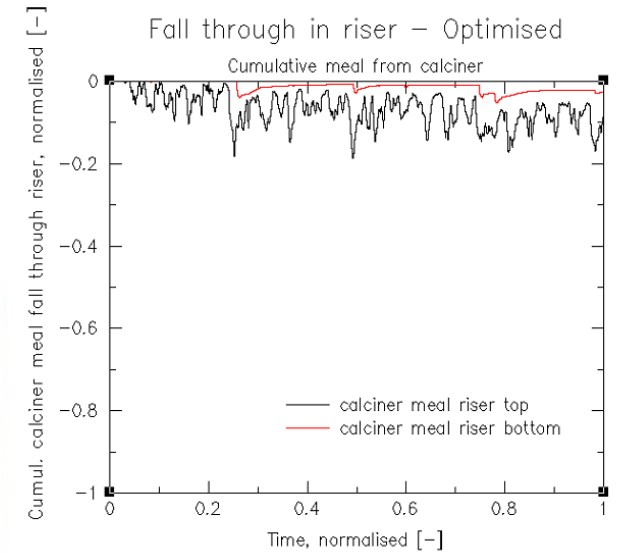
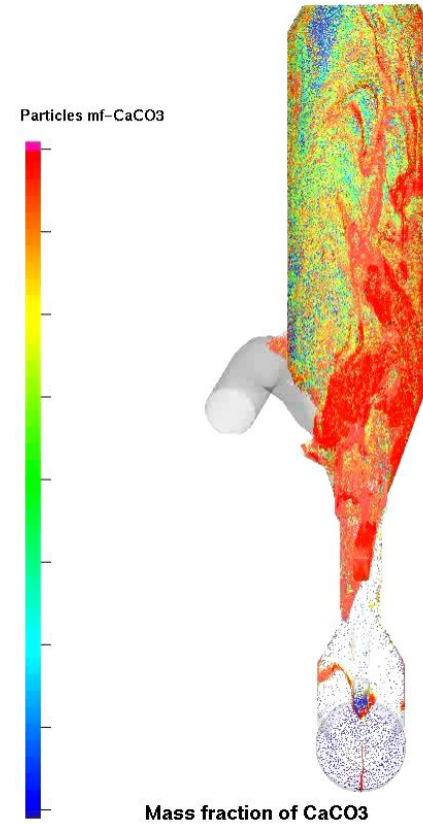


Calciner modelling - Meal fall-through

Basecase



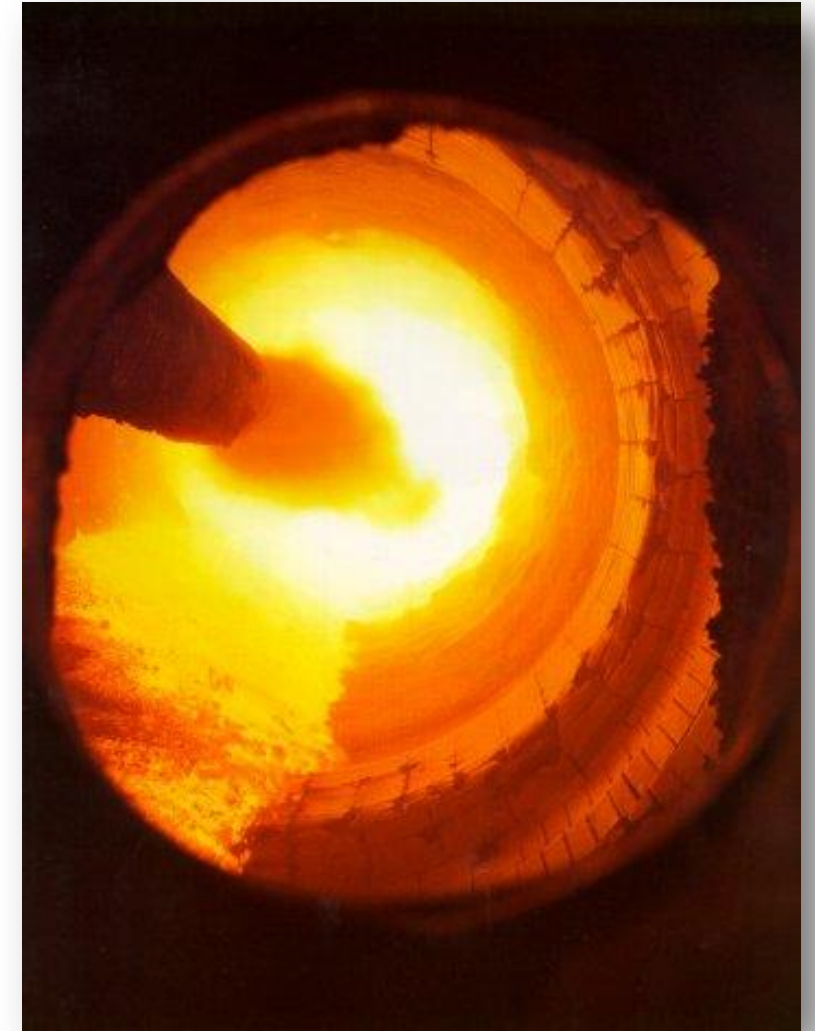
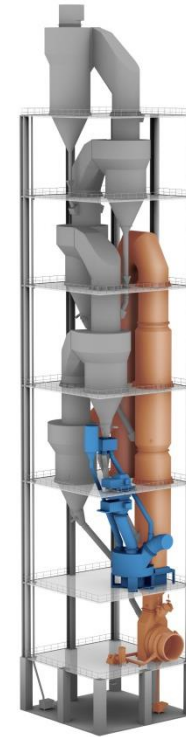
Optimised



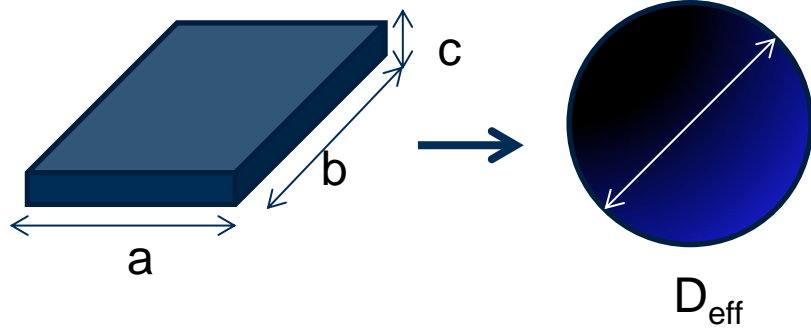
Challenges Alternative Fuels



Dry sewage sludge

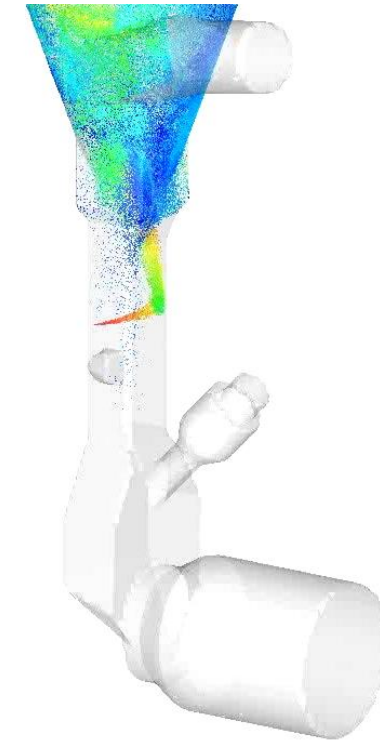
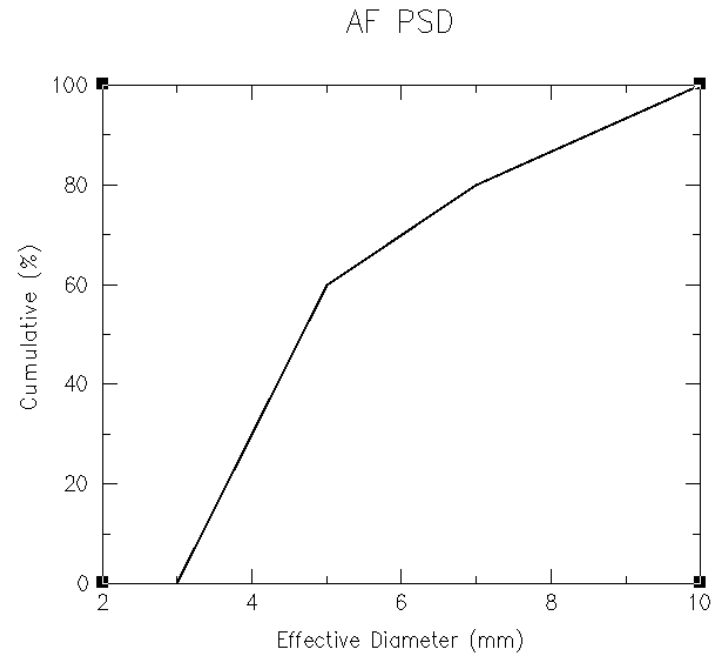


Challenges Alternative Fuels



a mm	b mm	c mm	Vol mm ³	D eff mm
10	10	0.5	50	4.57
20	20	0.5	200	7.26
30	30	0.5	450	9.51

$$D_{eff} = \sqrt[3]{\frac{6 \cdot VOL}{\pi}}$$



- ▮ Capture fall-through of solid particles in riser
 - ▮ Minimum cell resolution required in the riser
 - ▮ Small cells → small time-steps → long computational time
 - CPU only: 12-18 days for 80 simulation seconds
 - GPU 17.0.2: 4-8 days for 90 simulation seconds
- ▮ Postprocessing
 - ▮ Missing streamlines and pathlines in GMW
 - Needs VisIT, Ensight, Paraview, etc...
- ▮ Storage and Back-up
 - ▮ We generate 1 to 2 TB/month

Measurements

- ▀ Validation data difficult to obtain
 - ▀ Visual inspection
 - ▀ Estimation based on experience
 - ▀ Integral measurements
 - Temperature
 - O₂ contents
 - LOI
 - Mass balance

Modelling

- ▀ How to best define BC of raw meal?
- ▀ Predicted meal flow dependent of
 - ▀ Velocity
 - ▀ Distribution
 - ▀ pVoIF
 - ▀ Restitution coefficients (wall-particle)
 - ▀ Sensitive to inlet area

- Interpolate initialisation data from an IC file
 - save days of calculations with modified project
- Rotating domain (separators, crushers)
- Better capturing of complex internal geometry
- More predictable particle/wall interaction
- Better local mesh fineness control
 - Meshing is improved in VR17... still some “surprises”
 - Meal distribution box
 - Kiln feed from bottom stage
- Post-process results in CFD Post (ANSYS)
 - Export data as CGNS

- Barracuda used to make design decisions based on relative analysis
- Good collaboration with CFPD support
- Validation imperative
- Challenges with alternative fuels modelling
- Acquire more confidence in
 - Particle drag model
 - Meal inlet BC... before improving combustion model for sub stoichiometric conditions
- Drag model
 - EMMS delivers promising predictions. Compares best to measurements on
 - Lab-scale setup (without reactions)
 - Limited data available for industrial scale
 - Meal stream velocity and entrainment at site
 - Difficult to state that EMMS is the most adequate for industrial conditions
 - EMMS very sensitive to particle volume fraction
 - Meal blocks-up at vol. fraction well below max packing fraction

Thank you! Any Questions?

